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Title: Modeling Marangoni Effect in Liquid-Liquid Microfluidic Systems

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Modeling Marangoni Effect in Liquid-Liquid Microfluidic Systems

Alison Root

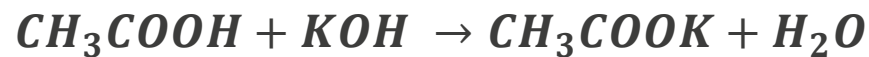
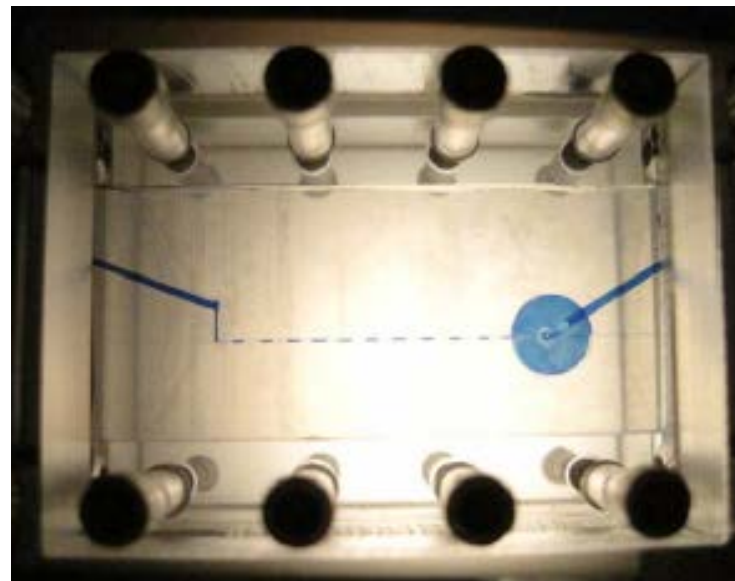
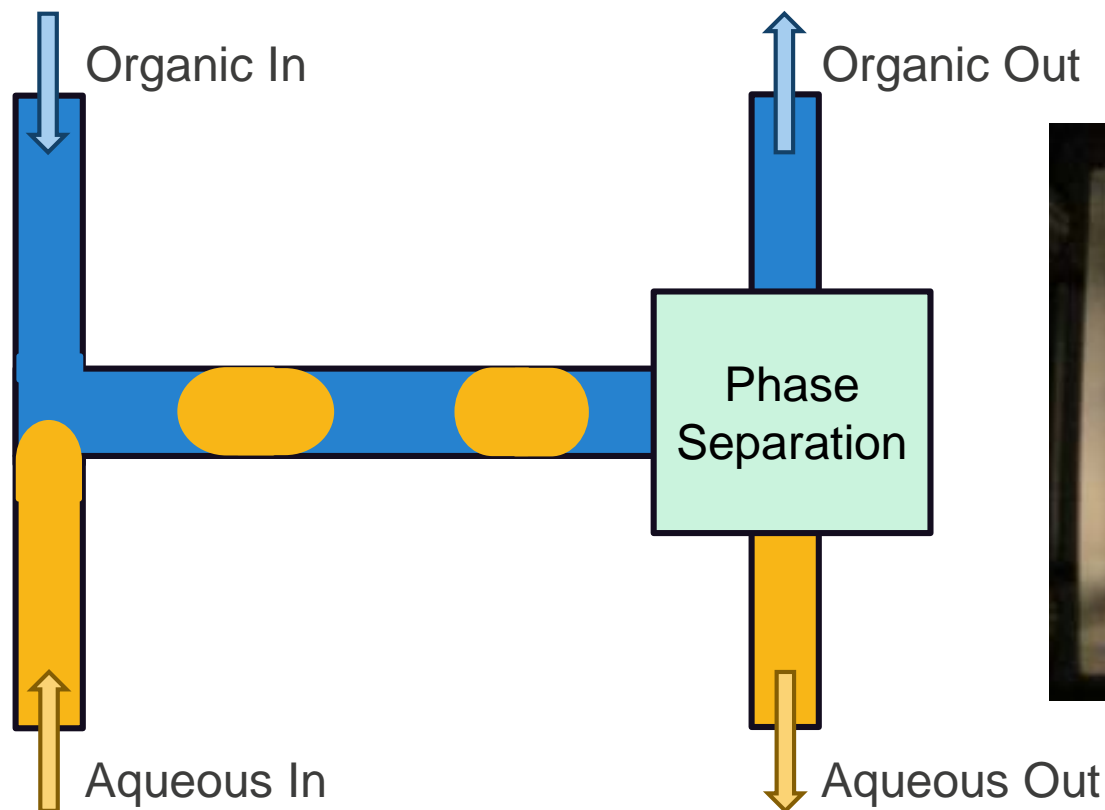
**Mentors: Garrison Stevens (MET-1)
and Scott Ouellette (W-13)**

August 2, 2017



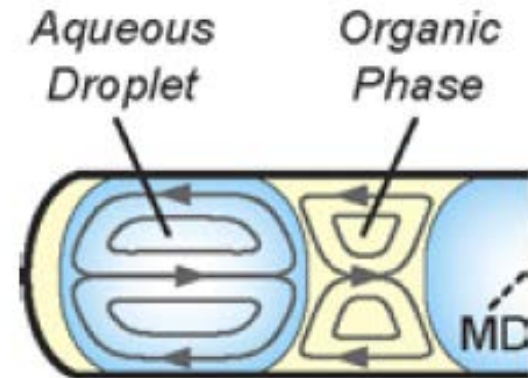
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Microfluidics presents opportunities for high mass transfer rates between fluids within a small device

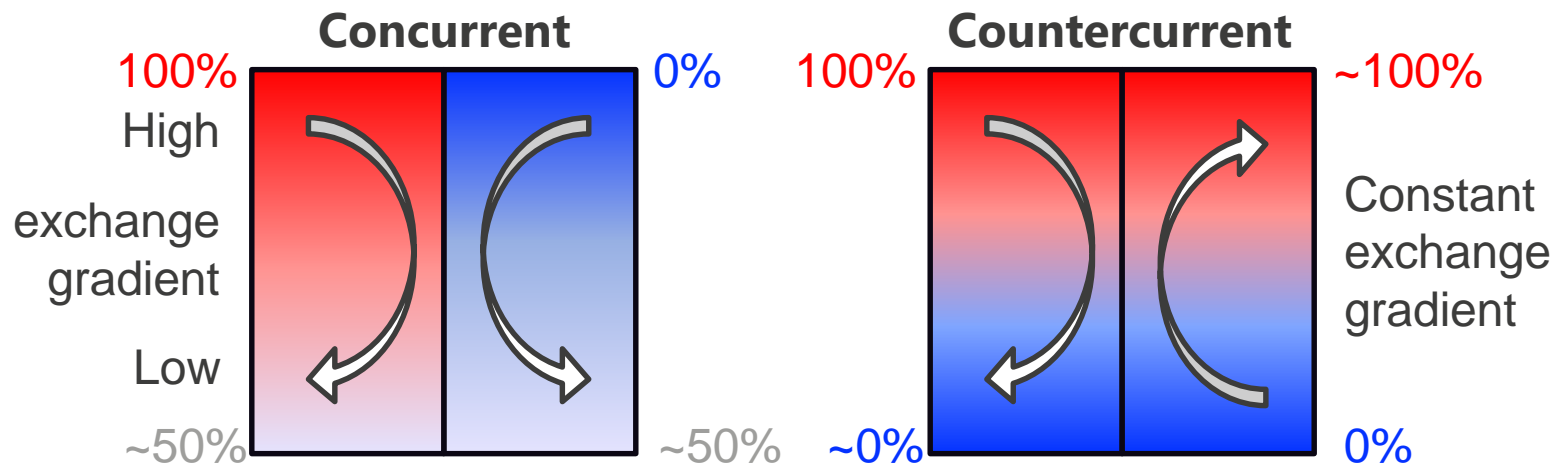


Benefits of droplets in a two-phase flow channel

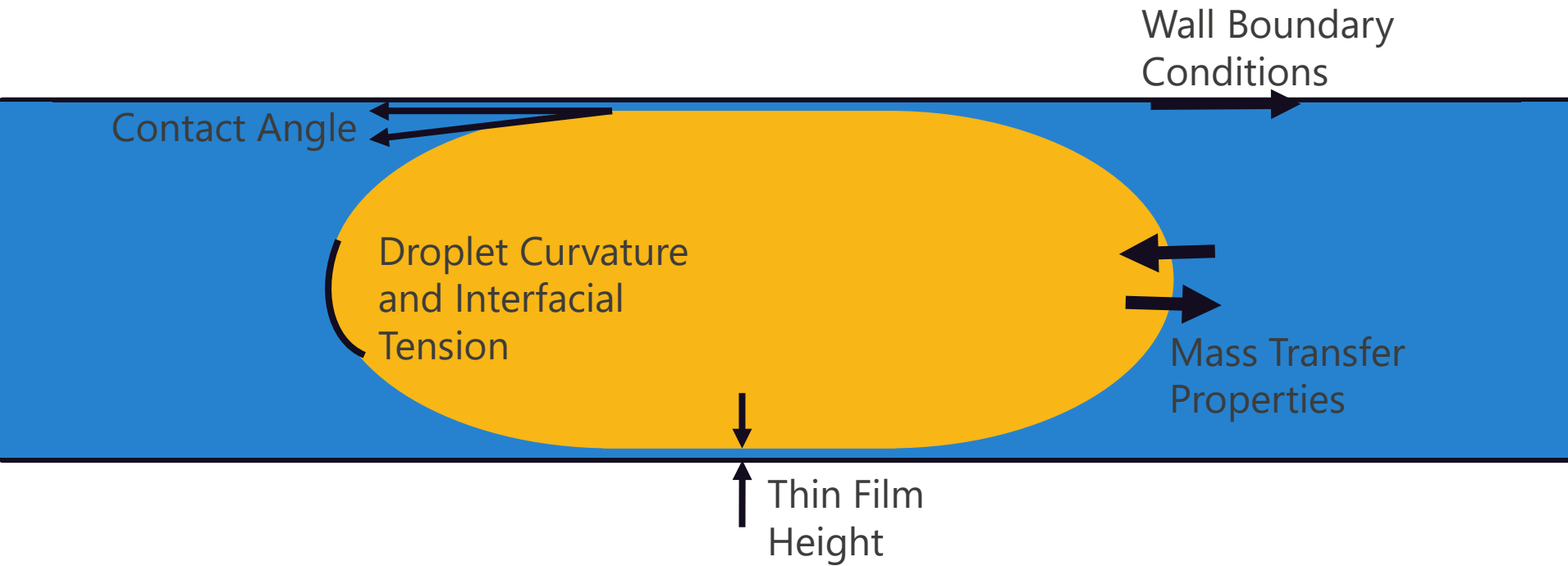
- Droplets are beneficial for mass transfer due to the maximal surface area between the two fluids and the development of countercurrent flow



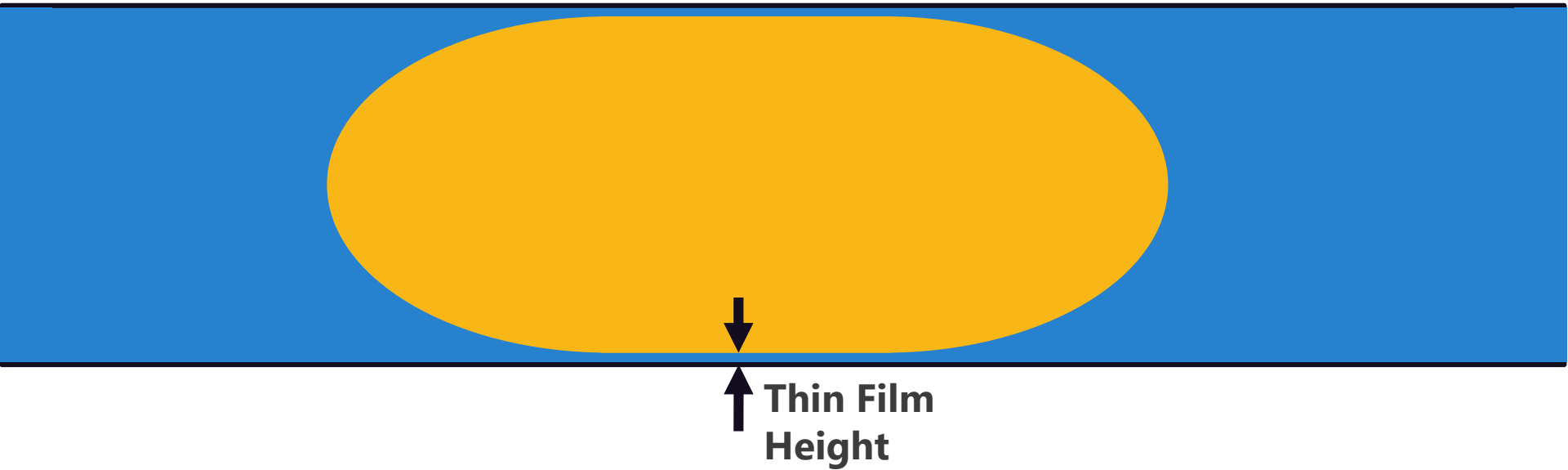
Flow inside individual "slugs"
Nichols, et al., J. Am. Chem. Soc., 133,
(2011), 15721-15729



Uncertain parameters and measurements of interest in the model

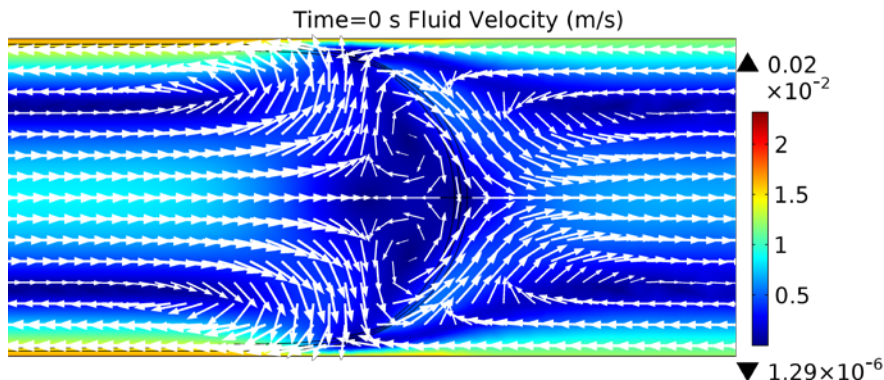
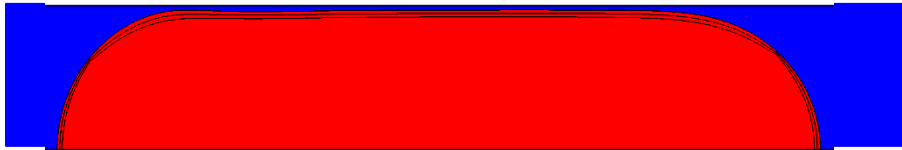
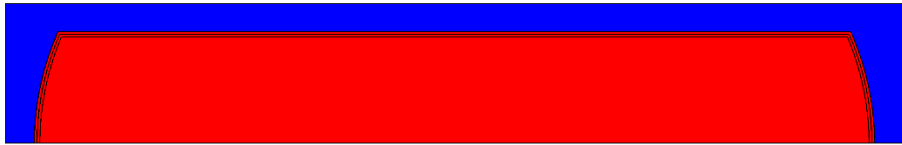


Uncertain parameters and measurements of interest in the model

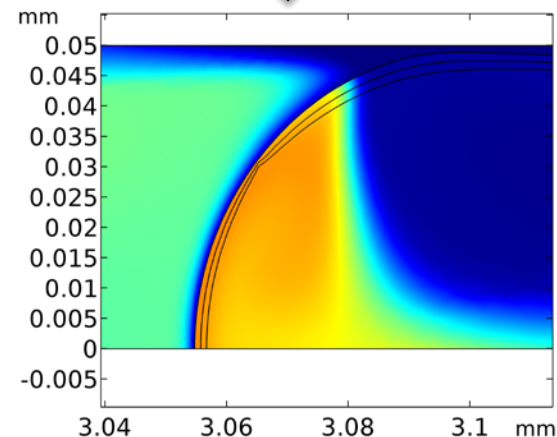
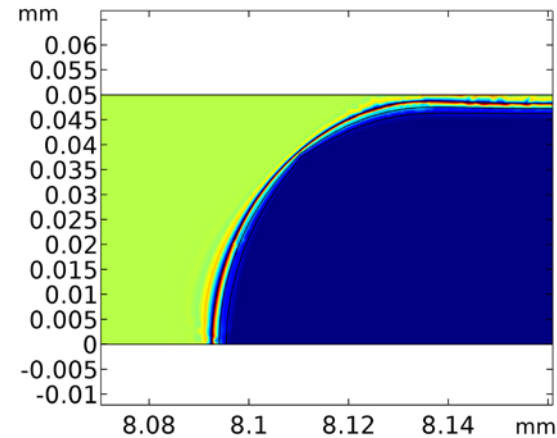


The model consists of two steps, one to establish fluid flow and droplet shape and one for mass transfer

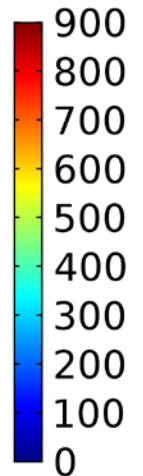
Moving Mesh



Mass Transfer

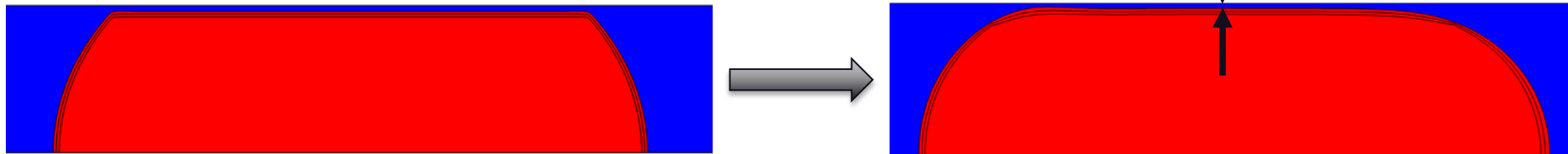


Acetic Acid
Concentration
(mol/m³)

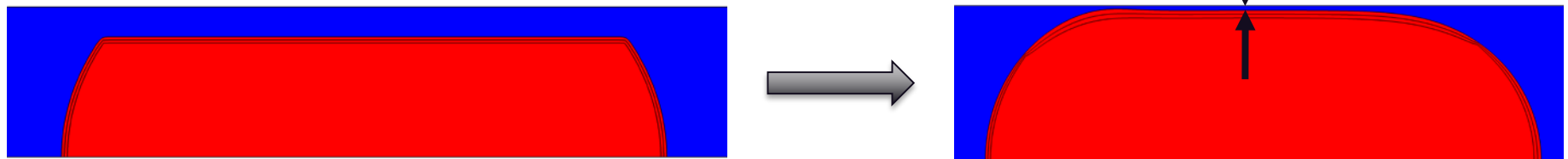


Converged droplet shape for initial length of 0.2 mm

Time (s)	Thin Film Height at Center (mm)	Droplet Length (mm)
0	0.001	0.202
0.5	0.01341	0.2084

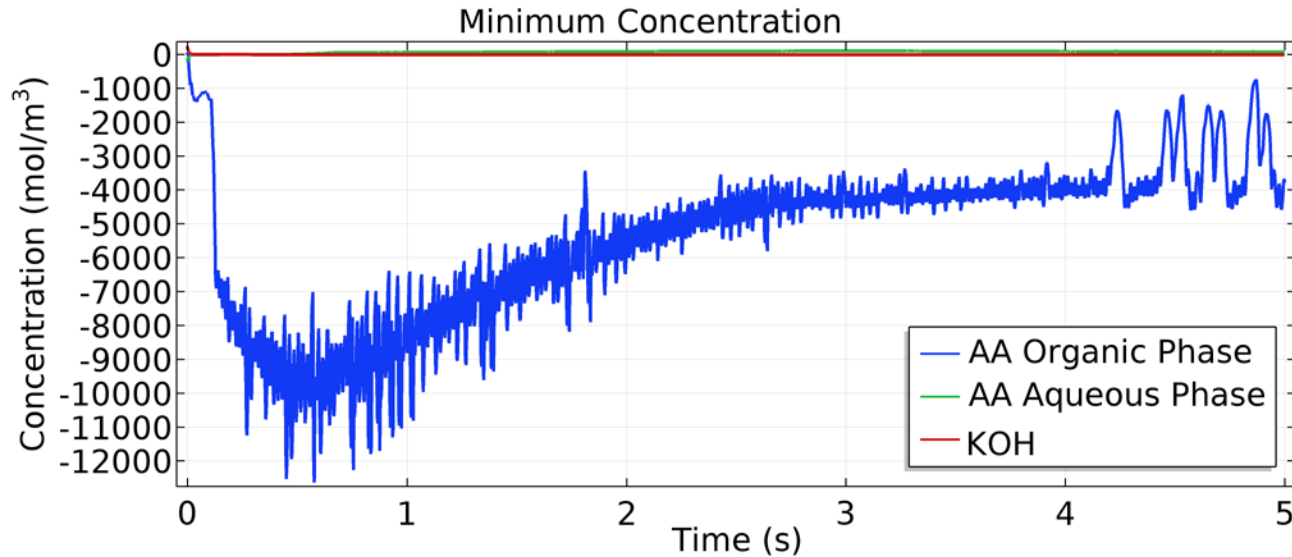


Time (s)	Thin Film Height at Center (mm)	Droplet Length (mm)
0	0.010	0.202
0.5	0.01505	0.1800

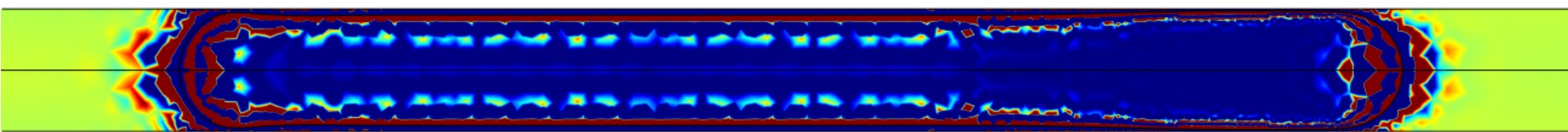


Numerical errors are common in convection and diffusion problems with sharp boundaries

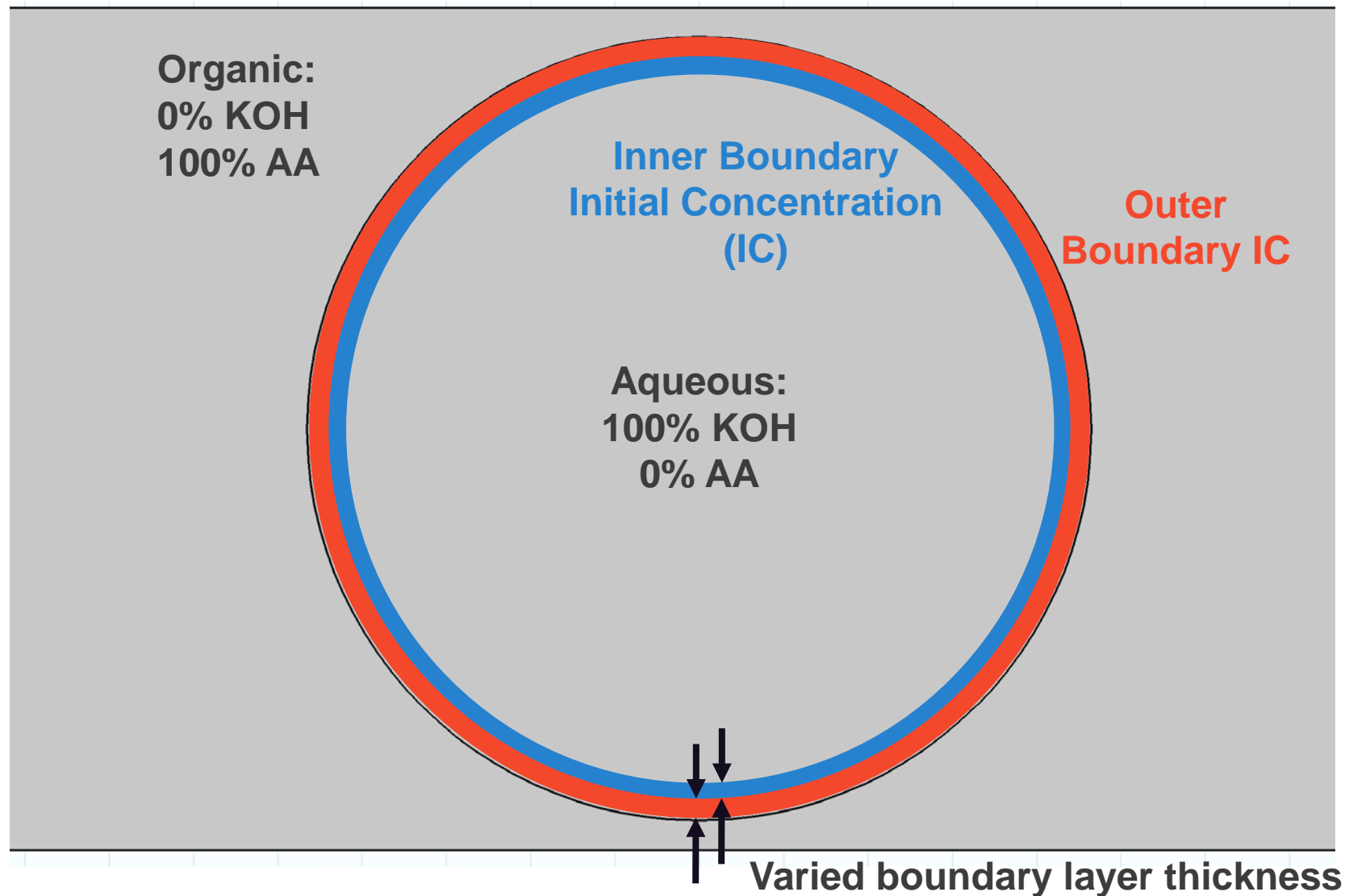
- Negative concentrations



- System mass not conserved
- Strange numerical behavior



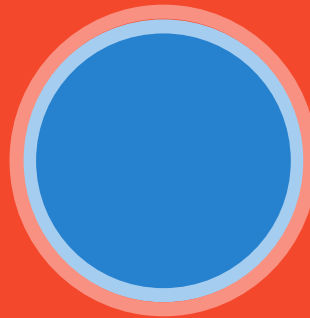
A toy model was investigated to look for ways of reducing numerical errors in the mass transfer



Several types of initial concentration conditions were tested with this model



Initial concentrations in original model (no boundary layers)

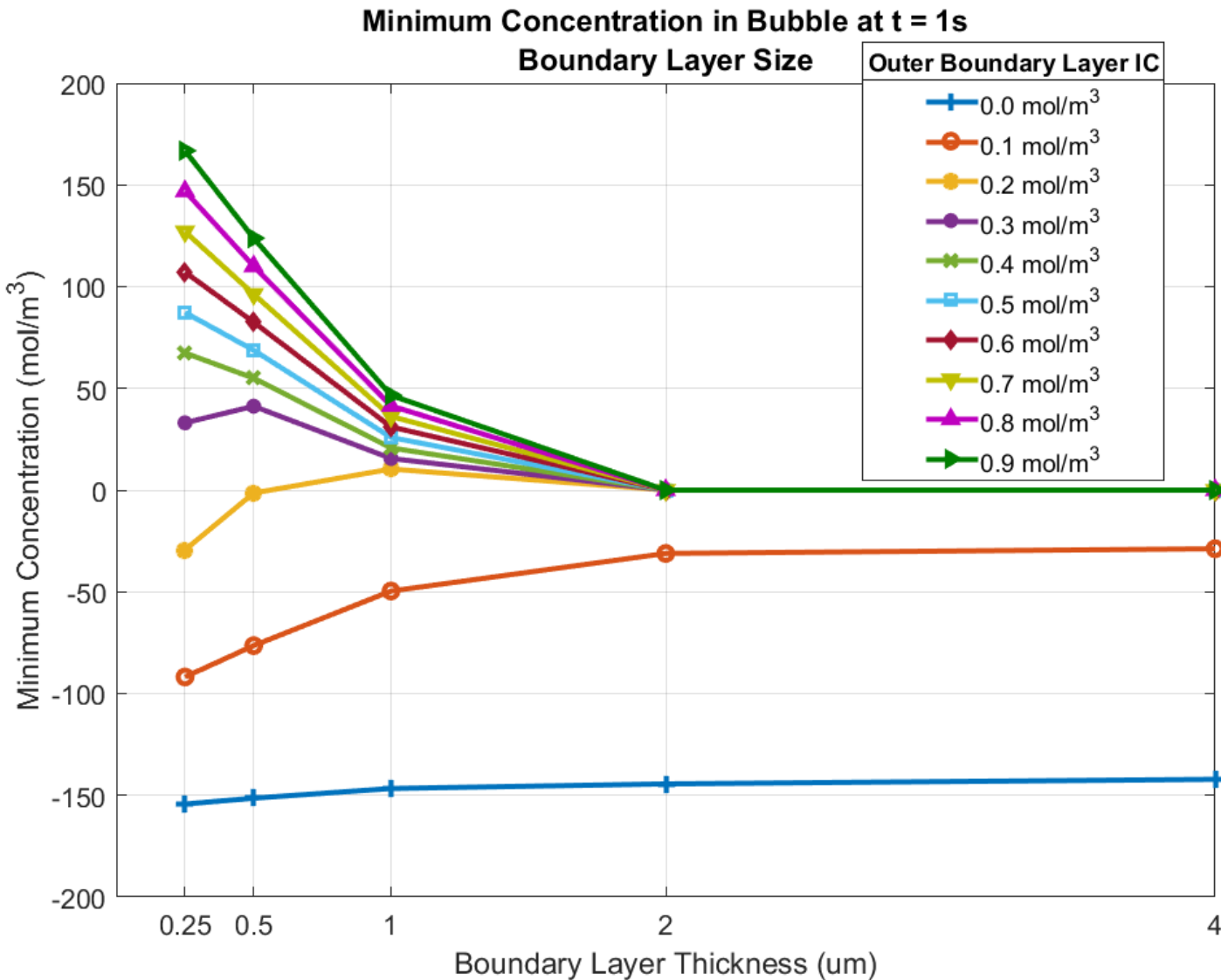


Initial concentrations with boundary layers



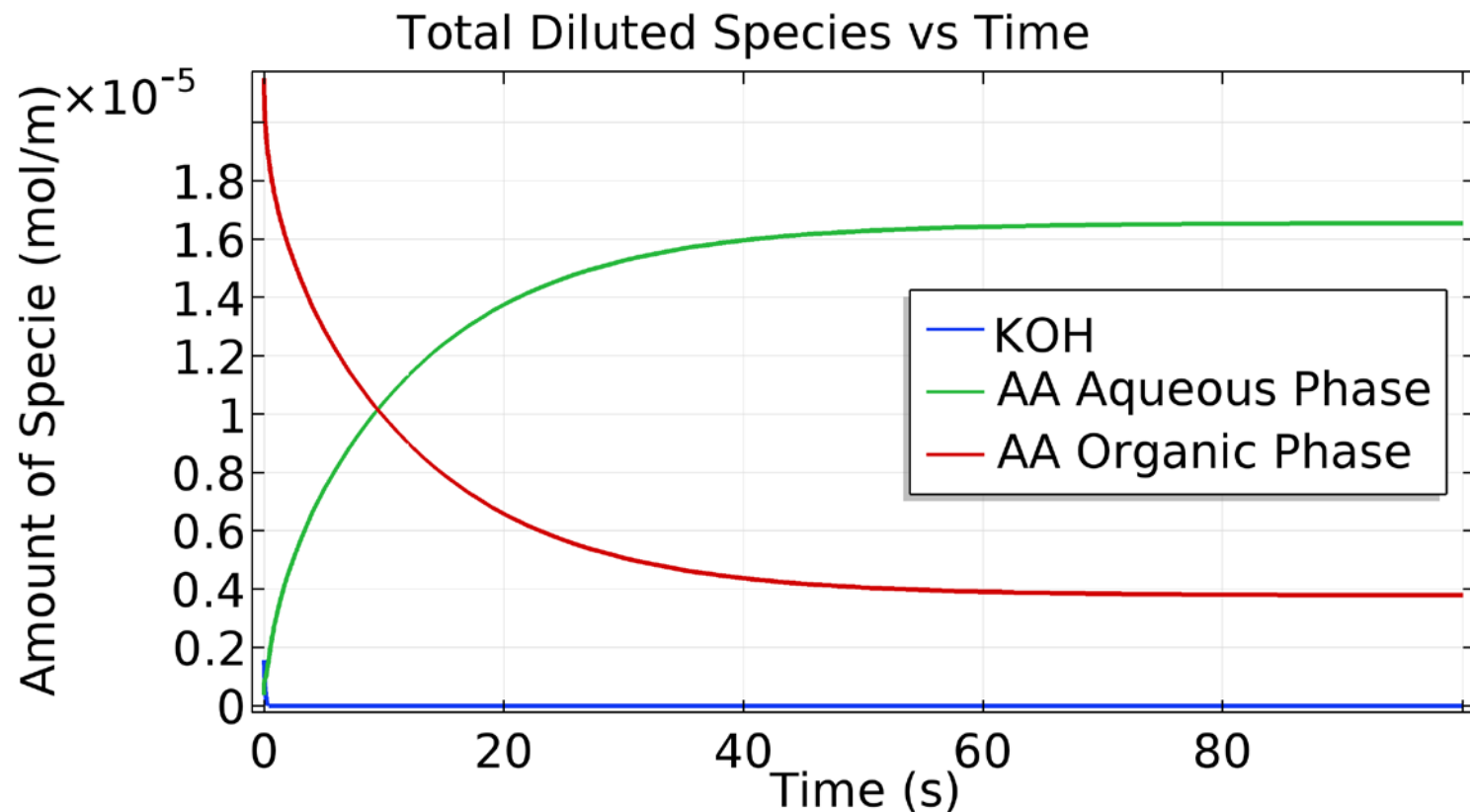
Initial concentrations with smoothing in boundary layers

Parametric studies of boundary layer thickness and concentrations in the toy model helped find ways to reduce numerical errors in the mass transfer

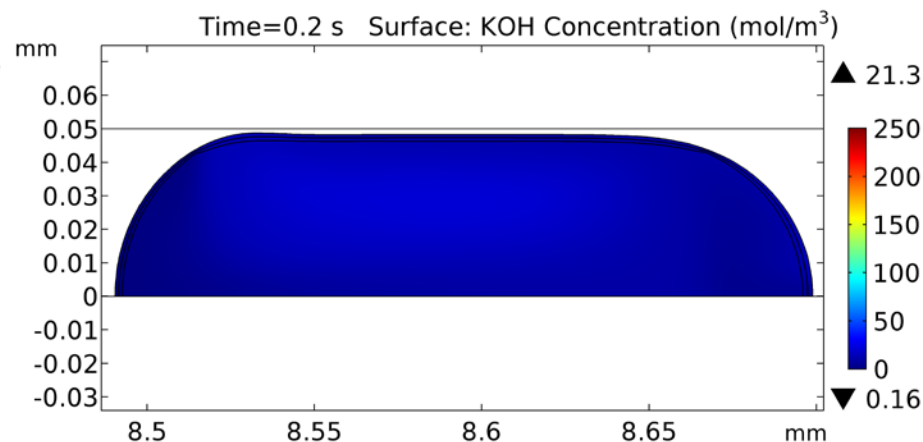
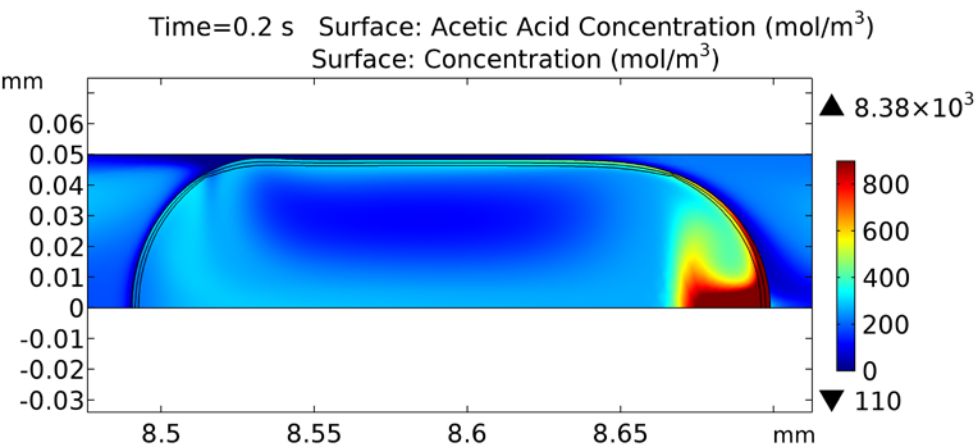
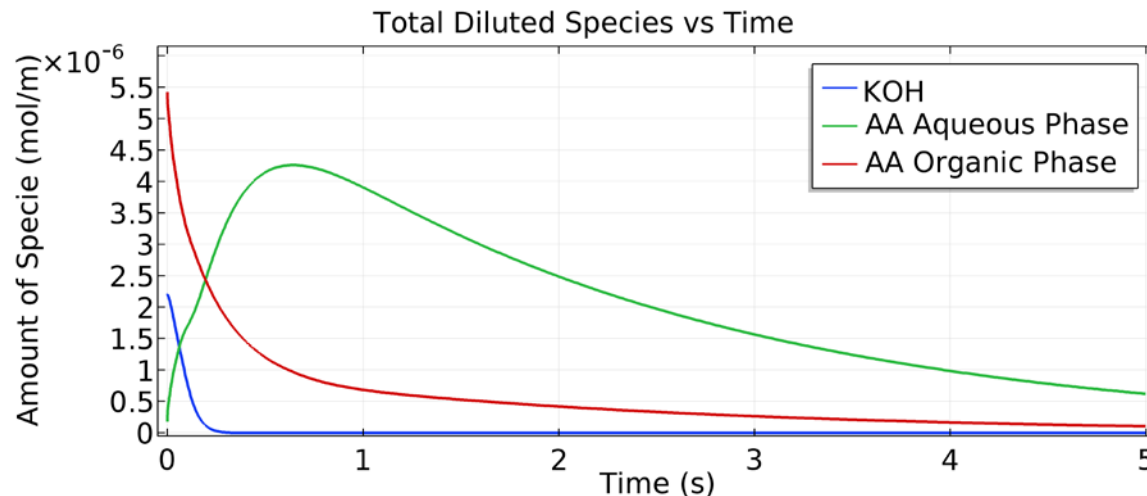
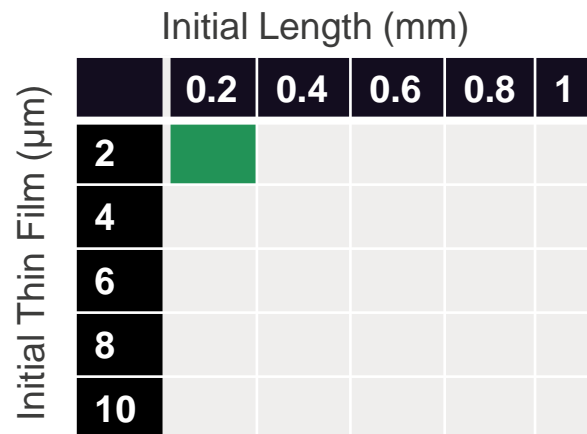


The behavior seen in the toy model using some combinations of parameters is what is expected from mass transfer

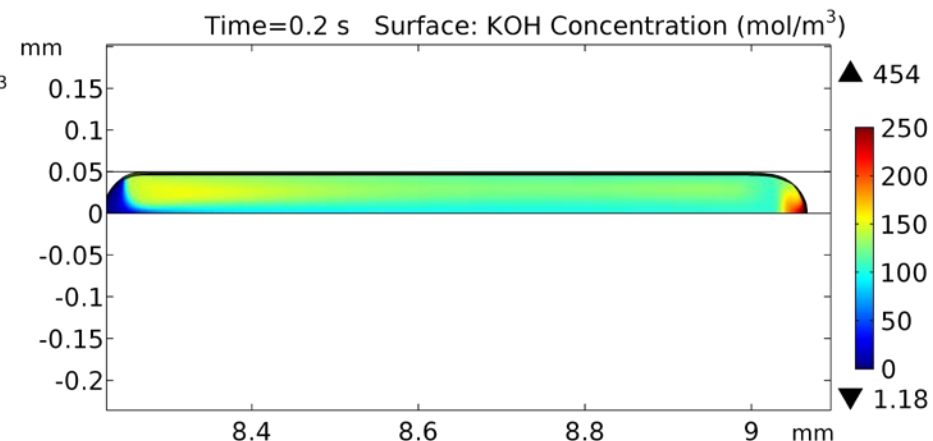
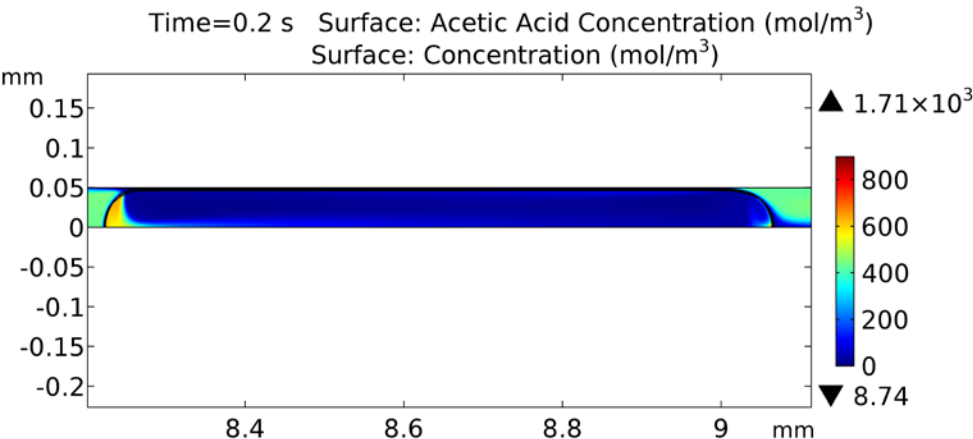
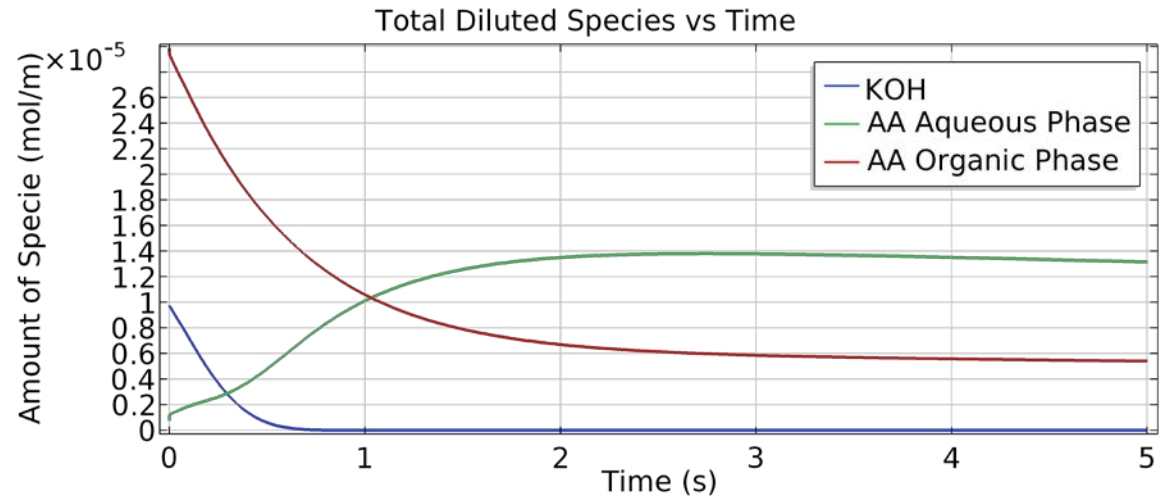
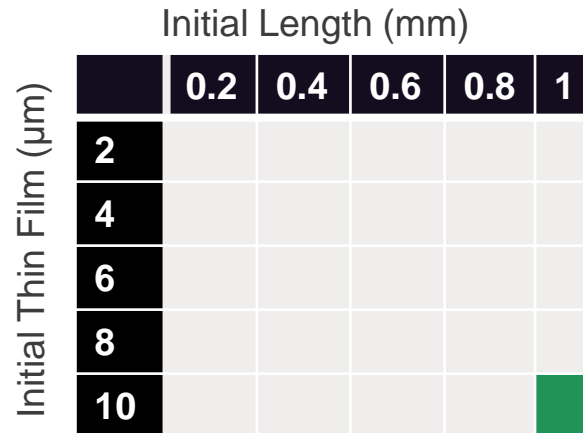
- Total acetic acid is constant after KOH has reacted away
- Parameters for this behavior:
 - Thicker boundary layers (at least 1 μm)
 - Outer boundary layer concentration at least 20% of concentration inside droplet



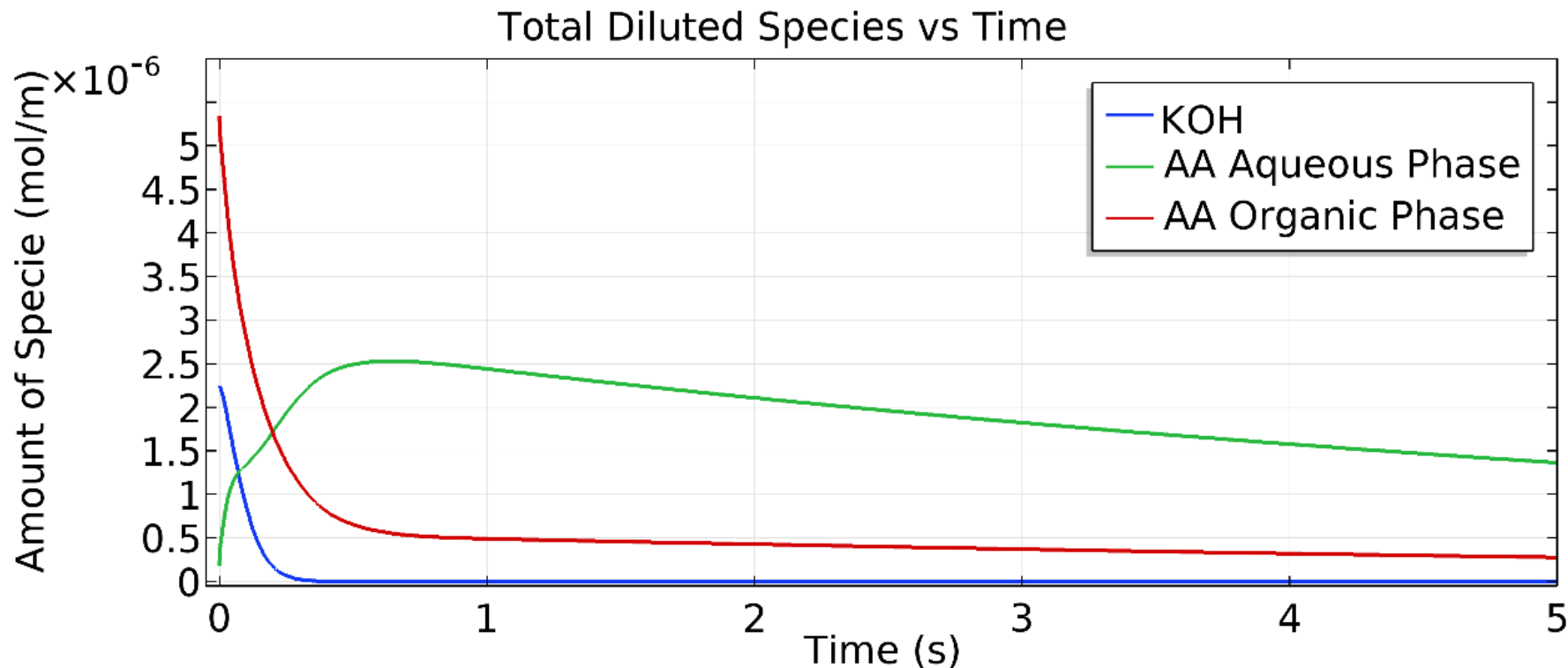
Using parameters that worked in the toy model gives better mass transfer results in the full-physics model



Again, changing initial thin film height but keeping length constant has a minimal effect on mass transfer

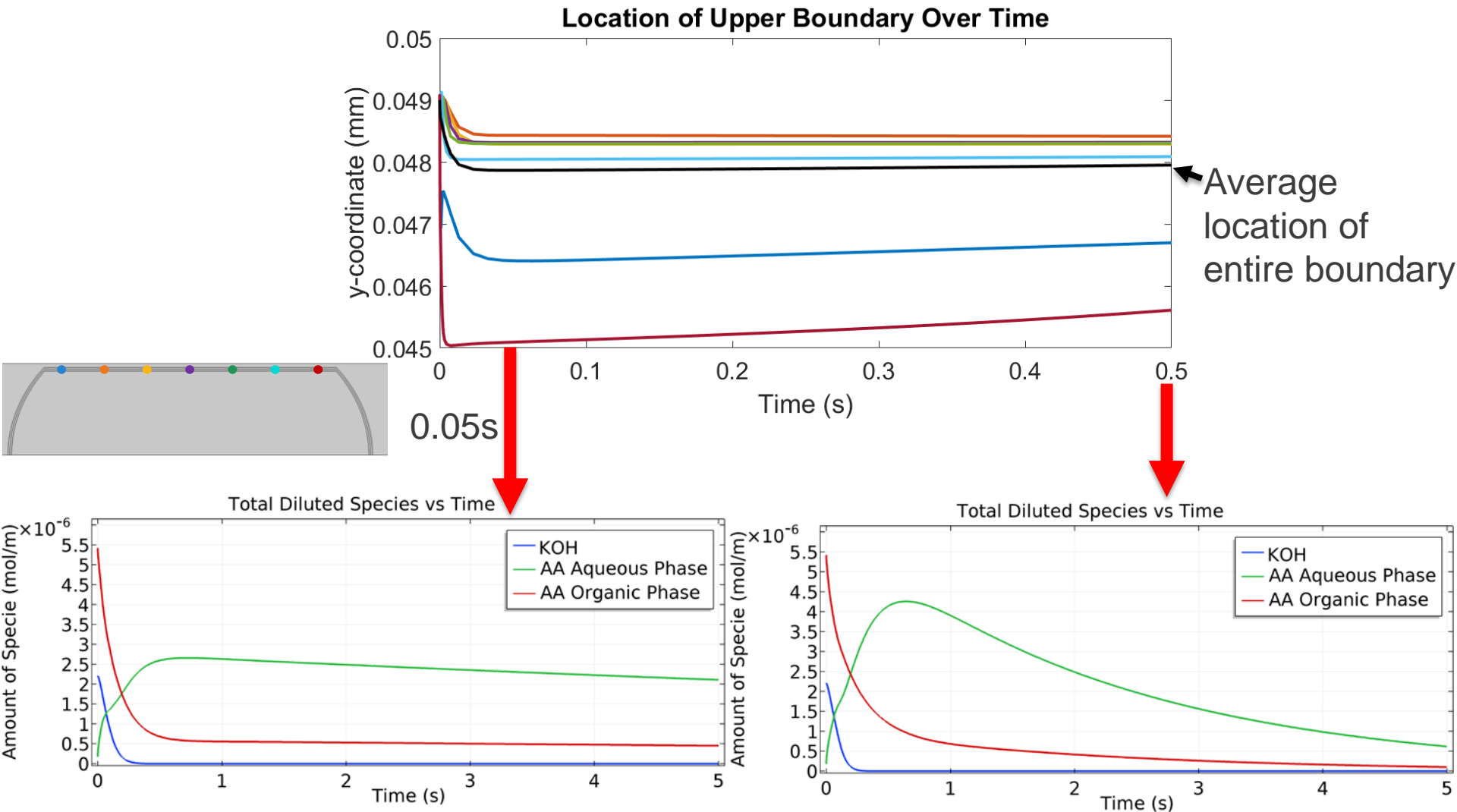


This version of the mass transfer step is much better than before, but there are still problems



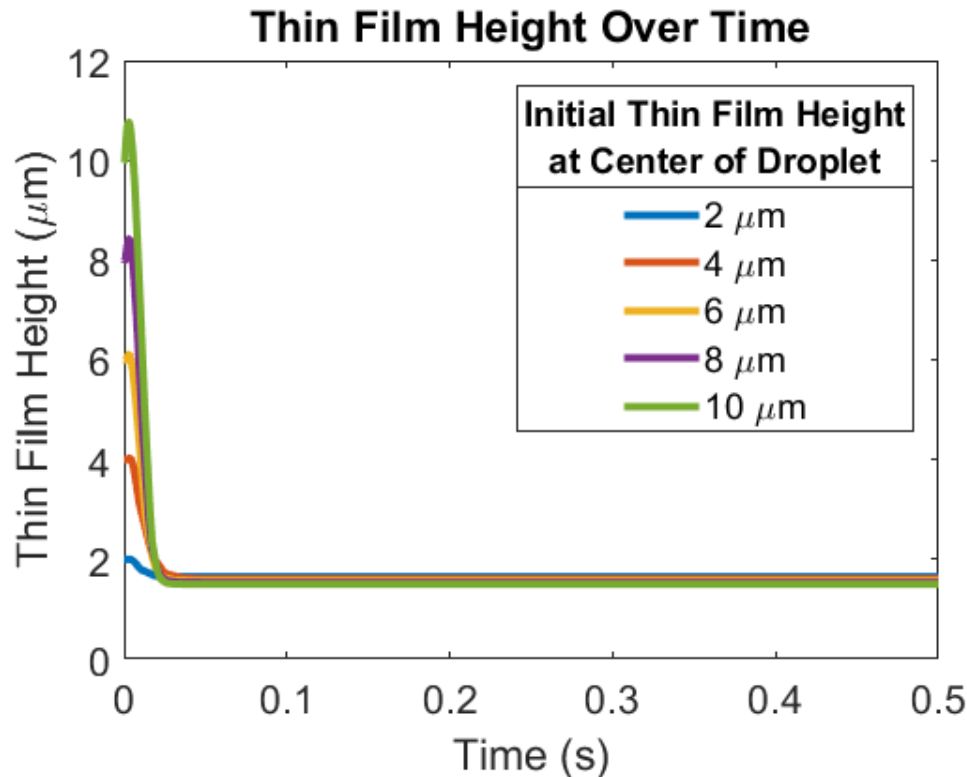
- **Conservation of mass is still not ensured**
- **Alleviated with more stable bubble, but still not perfect**
 - Can bubble not stabilize fully?
 - Is there some other problem?

When the droplet is in a more stable state from the moving mesh step, the mass transfer step is better



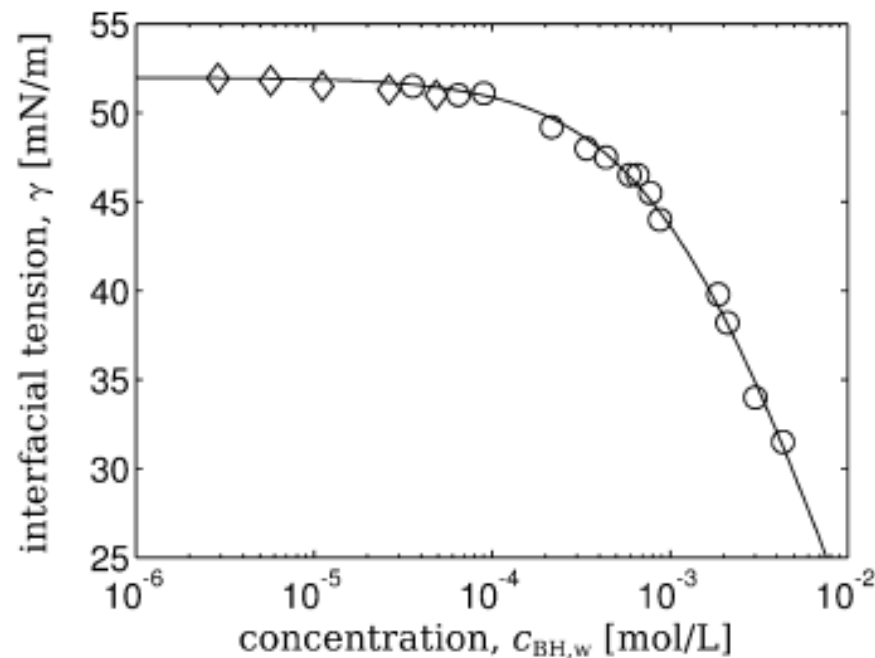
Conclusions

- Developed a droplet model that takes thin film height into account.
- Studied numerical errors in mass transfer models.
- Droplet tends to converge to a similar height at the same flow parameters regardless of initial size.
 - Can predict thin film height based on flow parameters



Future work

- Fix problem with acetic acid loss
- Combined model
 - One model that does moving mesh and mass transfer simultaneously
 - Mass transfer affects interfacial tension, but does interfacial tension affect droplet shape?



Fricke and Sundmacher.
Langmuir. **2012**. 28, 6803-6815.

Thank you!
Questions?

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